



Effect of Thermal Radiation on Heat Transfer of Ferrofluid Over a Stretching Cylinder with Convective Heating

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Abstract

In view of this we scrutinize the numerical solution using the Kellor box method for the natural differential equations which describes the MHD flow of ferrofluid over a stretching cylinder with thermal radiation and convective heating. Water as convective base fluid containing nano particles of magnetite (Fe_3O_4) is taken up. Comparison between magnetite (Fe_3O_4) and non-magnetic (Al_2O_3) nanoparticles is also made. The relevant physical parameters appearing in velocity and temperature distributions are analyzed and examined with the help of Fig.s. To examine the correctness of the method an analogy has been made with some earlier published results. It is noticed that by increase the strength of magnetic field, the percent difference in the heat transfer rate of magnetic nano particles with Al_2O_3 decrease. Further, convective heating and thermal radiation are highly influenced the temperature distribution of the ferrofluid.

Keywords: Ferrofluid, stretching cylinder, MHD, convective heating, thermal radiation.

1. Introduction

The detailed examination of Nanofluids has been subjected of covering and exploring the aftereffect or consequences of rising thermal conductivity heat transfer procedure. Nanofluid is propose to refer a fluid in that nanometer-magnitude molecules are suspended in classical heat transfer absolutely necessary fluids [1,2]. The fluids which are considered as bad transfer of heat are Water, encom-passing oil, and ethylene glycol. In various engineering applications like microelectronics, heat interchangers, refrigerating of electronic apparatus Nanofluids are used. A guanine studies of this wonderful topic together with the theoretical as well as experimental data can be much benefited in the literature [3-11]. More precisely In non-conducting liquids such as heptanes, water, kerosene, and hydrocarbons, the magnetic Nanofluids (Ferro fluids) those are colloidal suspension of magnetic nano particles like cobalt, ferrite, magnetite are dispersed. Ferrofluids are quite useful to explain different engineering applications like drug targeting technology, mega-phones, rotary shaft seals and bumpers. In the literatures [4-15] we can found the dissimilar applications of ferrofluids if we observe it in detailed. The impact of nanoparticle migration on thermal performance of ferrofluid flow inside a vertical micro ring examine by Malvandi et al [16], a few days ago. Heysiattalab et al [17] deeply examine the anisotropic approach of ferrofluids at film wise amplification on a vertical plate with a changeable directional magnetic field. Nanoparticle migration effects, and thee condensate falling film of ferrofluids in the presence of anisotropic behavior of thermal conductivity is analysed theoretically by Malvandi et al [18]. Rashad [19] was observed that the consequence of partial slip over a MHD flow of mixed convection of ferrofluid on a radiating wedge of non-isothermal. In another study, In the presence of slip effect how the boundary layer of a ferro fluid flows on semi infinite inclined plate also studied by Rashad [20].

The processes having high temperature like nuclear reactors, combustion turbines and storage of thermal energy etc... the analysis of heat transfer by convection accompanied by thermal radiation has more significance. In the work [21] the authors were explored the thermal radiation effects based on Rooseland diffusion approximation over a combined convection across vertical plate with free stream of uniform surface temperature and uniform velocity. The thermal radiation of gray fluid that emits as well as absorbs radiation in a non-scattering medium was examined in [22]. Authors in [23] were examined the radiative flow in the existence of magnetic field. The authors in [24] were explained the impact of thermal radiation on the boundary layer flow by an exponentially stretching sheet. The authors of [25] examined the impact of thermal radiation on MHD flow of a second grade fluid. In [26] the authors were assessed that the consequences of radiation over natural streamline flow from a horizontal circular cylinder. Finally it was concluded that increase in radiation results increase in velocity as well as thermal boundary layer thickness. Ahmad et al. [27] examined the influence of thermal radiation over mixed convection boundary layer flow of a visco elastic fluid over a circular cylinder with constant surface temperature.

By the work of Aziz [28], on the boundary layer flow with convective surface boundary condition have acquired more attentiveness, in recent years. In this work he also explored by connective surface boundary condition the thermal boundary layer flow over a flat plate. Afterwards Makinde and Aziz [29] together by taking the same connective boundary conditions they explained the boundary layer flow of a nanofluid past over a stretching sheet. Shehzad et al. [30] by using convective surface boundary conditions explained exact solution of three-dimensional flow of Jeffery fluid. Hayat et al.[31], by using convective surface boundary conditions he scrutinized the three dimensional boundary layer flow of Maxwell fluid on stretching surface. Zaih et al. [32] studied the effect of thermal radiation and convective boundary conditions on William son fluid over an exponentially stretching sheet.



So far no studies have been made to scrutinize the out-turn of thermal radiation on MHD boundary layer flow of a ferrofluid on stretching cylinder with convective heating. The Keller box method used gives us a numerical solution of the equation obtained. This only describes the problem, after similarity functions. The effects of the embedded flow controlling parameters on various issues like fluid velocity, temperature skin friction and heat transfer rate revealed in the similarity solution presented in order to predict heat transfer characteristics. A comparative study is also presented below.

2. Mathematical Analysis

Take a ferrofluid, In that we introduce a cylinder. Suppose the radius of cylinder is 'a', here it is assumed that the cylinder is stretching along its axis. The velocity of the fluid, $U_w = U_0$, the heat flux on the cylinder surface is $q_w = T_0$, and U_0, T_0 are the functions of $\frac{x}{l}$. A boundary layer is formed on the circular

cylinder. Suppose the uniform magnetic field of intensity B_0 acts along the radial direction due to this assumption for small magnetic Reynolds number the impact of induced magnetic field is almost negligible. Now the above system is explained by the following equations

$$\frac{\partial}{\partial x}(ru) + \frac{\partial}{\partial r}(rv) = 0 \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial r} = \frac{\mu_{nf}}{\rho_{nf}} \left(\frac{\partial^2 u}{\partial r^2} + \frac{1}{r} \frac{\partial u}{\partial r} \right) - \frac{\sigma_{nf}}{\rho_{nf}} B_0^2 u \quad (2)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial r} = \frac{k_{nf}}{(\rho c_p)_{nf}} \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} \right) - \frac{1}{(\rho c_p)_{nf}} \frac{\partial q_r}{\partial r} \quad (3)$$

The boundary conditions are

$$u = U_w, \quad v = 0, \quad k_f \frac{\partial T}{\partial r} = -q_w \quad \text{at } r = a \quad (4)$$

$$\frac{\partial T}{\partial r} = -h_s(T - T_\infty)$$

$$u \rightarrow 0, \quad T \rightarrow T_\infty \quad \text{as } r \rightarrow \infty \quad (5)$$

The radiative heat flux q_r is simplified by the Rosseland diffusion approximation [33] as

$$q_r = \frac{-4\sigma}{3(\alpha_s + \sigma_s)} \frac{\partial T^4}{\partial r} \quad (6)$$

Where σ is the Stefan-Boltzmann constant, α_r is the Rosseland mean absorption factors and σ_s is the scattering factor. Let us consider that the fluid-phase temperature differences within the flow are sufficiently small as reported in the work [34]. So that T^4 may be expanded as a linear function of temperature T and neglecting higher order terms as

$$T^4 \approx 4T_\infty^3 T - 3T_\infty^4 \quad (7)$$

Now expression (5) reduces to the form

$$q_r = \frac{-16\sigma T_\infty^3}{3(\alpha_s + \sigma_s)} \frac{\partial T}{\partial r} \quad (8)$$

It is worth mentioning here that use of the Rosseland diffusion approximation is valid the interior of a medium but it is not employed near the boundaries. It is good only from optically thick boundary layer. Since expression (8) does not contain any term for the radiation from the boundary surface therefore is not valid to predict a complete description of this physical situation near the surface. In the other words the boundary surface effects are negligible in the interior of an optically thick boundary layer region. Which is due to the fact that the radiation from the boundaries becomes very weak before reaching the interior.

In the above q_r is radiative heat flux, h_s is the convective heat transfer coefficient, r, x are axial and radial coordinates of the cylinder respectively, u, v are the velocity components along x and r directions. T is temperature, ρ_{nf}, μ_{nf} and α_{nf} are the density, dynamic viscosity, thermal diffusivity of the nanofluid respectively is given by

$$\begin{aligned} \mu_{nf} &= \frac{\mu_f}{(1-\phi)^{2.5}}, \quad \rho_{nf} = (1-\phi)\rho_f + \phi\rho_s \\ (\rho c_p)_{nf} &= (1-\phi)(\rho c_p)_f + \phi(\rho c_p)_f, \quad \nu_{nf} = \frac{\mu_{nf}}{\rho_{nf}} \end{aligned} \quad (9)$$

$$\frac{k_{nf}}{k_f} = \frac{(k_s + 2k_f) - 2\phi(k_f - k_s)}{(k_s + 2k_f) + \phi(k_f - k_s)}, \quad \alpha_{nf} = \frac{k_{nf}}{(\rho c_p)_{nf}}$$

In the above equations, ρ_s is the reference density of the solid fraction, ρ_f is the reference density of the fluid fraction, k_s is the thermal conductivity of the solid fraction, c_p is the specific heat at constant pressure, μ_f is the viscosity of the fluid fraction, Φ is the solid volume fraction of a nano fluid, and k_{nf} is the thermal conductivity of the nano fluid.

The following variables are defined

$$\eta = \frac{r^2 - a^2}{2a} \left(\frac{U_w}{\nu_f x} \right)^{1/2}, \quad \psi = (\nu_f U_w x)^{1/2} \text{af}(\eta), \quad \theta = \frac{T - T_\infty}{T_f - T_\infty} \quad (10)$$

Here the stream function is ψ . which defined as $u = r^{-1} \frac{\partial \psi}{\partial r}$

and $v = -r^{-1} \frac{\partial \psi}{\partial x}$ this satisfies the equation of continuity.

$$\begin{aligned} (1 + 2\gamma)\eta^4 + 2\gamma\eta^2 + (1 - \Phi)^{2.5} \left[1 - \Phi + \Phi \left(\frac{\rho_s}{\rho_f} \right) \right] (\eta^2 - 1)^2 \\ - (1 - \Phi)^{2.5} Mf' = 0 \end{aligned} \quad (11)$$

$$\left(\frac{k_{nf}}{k_f} \right) \frac{1}{\text{Pr}} \left(1 + \frac{4}{3} \text{Rd} \right) [(1 + 2\gamma\eta)\theta'' + 2\gamma\theta']$$

$$+ \left[1 - \Phi + \Phi \frac{(\rho_{cp})_s}{(\rho_{cp})_f} \right] (f\theta' - f'\theta) = 0 \tag{12}$$

$$f(0) = 0, f'(0) = 1, \theta'(0) = Bi(1 - \theta(0)) \tag{13}$$

$$f' \rightarrow 0, \theta \rightarrow 0 \text{ as } \eta \rightarrow \infty \tag{14}$$

Here Pr is the Prandtl number, M is the Magnetic parameter, γ Curvature parameter, Rd is the radiation parameter and Bi is local Boit number.

$$\gamma = \left(\frac{1\nu_f}{U_0 a^2} \right)^{1/2}, Pr = \frac{\mu_f(\rho_{cp})}{\rho_f k_f}, M = \frac{\sigma_{nf} B_0^2 l}{\rho_f U_0}$$

$$\beta = \delta \left(\frac{U_0}{1\nu_f} \right), Rd = \frac{-4\sigma T_\infty^3}{k_f(\alpha_r + \sigma_s)}, Bi = h_s \frac{a}{r} \sqrt{\frac{\nu_f x}{U_w}} \tag{15}$$

We know that $\gamma = 0$ and $\gamma = 1$ for plate and cylinder respectively. C_f is called skin friction coefficient and Nu_x is local Nusselt number. These quantities can be written as

$$C_f = \frac{\tau_w}{\rho_f U_w^2}, Nu_x = \frac{x q_w}{k_f (T_f - T_\infty)} \tag{16}$$

Here q_w is heat flux from the plate, τ_w is the skin friction those values are

$$\tau_w = \mu_{nf} \left(\frac{\partial u}{\partial r} \right)_{r=a}, q_w = -k_f \left(\left(1 + \frac{16\sigma T_\infty^3}{3(\alpha_r + \sigma_s)} \right) \frac{\partial T}{\partial r} \right)_{r=a}$$

We have

$$Re_x^{1/2} C_f = \frac{1}{(1-\Phi)^{2.5}} f''(0)$$

$$Re_x^{-1/2} Nu_x = \frac{-k_{nf}}{k_f} \left(1 + \frac{4}{3} Rd \right) \theta'(0) \tag{17}$$

For a pure fluid $\Phi = 0$, In the absence of slip condition $\beta = 0$ and magnetic field $M = 0$.

3. Solution of the Problem

Substitute the above values in equations (11) and (12), we have $(1+2\gamma\eta)f'''+2\gamma f''+(1-\Phi)^{2.5} A_1(f f''-f'^2)-(1-\Phi)^{2.5} M f' = 0$ (18)

$$A_3 \frac{1}{Pr} \left(1 + \frac{4}{3} Rd \right) [(1+2\gamma\eta)\theta''+2\gamma\theta'] + A_2(f\theta'-f'\theta) = 0 \tag{19}$$

Finite difference method:

$$A_1 = (1 - \Phi)^{2.5}, A_2 = (1 - \Phi) + \Phi \frac{\rho_s}{\rho_f}$$

$$A_3 = \frac{k_{nf}}{k_f}, A_4 = (1 - \Phi) + \Phi \frac{(\rho_{cp})_s}{(\rho_{cp})_f}$$

In order to solve the above equations (18)-(19), we are using new dependent variables $p(\eta), q(\eta), \theta(\eta)$, and $t(\eta)$ such that

$$f' = p, p' = q, \theta' = t \tag{20}$$

$$[(1+2\gamma\eta)q'+2\gamma q] + A_1 A_2 \left[\frac{fq}{2} - p^2 \right] - A_1 M p = 0$$

$$(21)$$

$$\left(A_3 + \frac{4}{3} Nr \right) [(1+2\gamma\eta)t'+\gamma t] + (A_3\gamma t) + \frac{Pr}{2} \cdot A_4 ft = 0$$

$$(22)$$

Now the boundary conditions () becomes

$$p(0)=1, f(0)=0, \theta(0)=1$$

$$p(\eta) \rightarrow 0, \theta(\eta) \rightarrow 0, \text{ as } \eta \rightarrow \infty \tag{23}$$

Define

$$\eta_0 = 0, \eta_j = \eta_{j-1} + h_j, \eta_J = \eta_\infty$$

Where the segment $\eta_{j-1}\eta_j$ with midpoint $\eta_{j-\frac{1}{2}}$, h_j as $\Delta\eta$ -

spacing and index $j = 1, 2, \dots, J$

The finite difference approximations for the equations (20) to (22) are

$$f_j - f_{j-1} - \frac{1}{2} h_j (p_j + p_{j-1}) = 0 \tag{24}$$

$$p_j - p_{j-1} - \frac{1}{2} h_j (q_j + q_{j-1}) = 0 \tag{25}$$

$$\theta_j - \theta_{j-1} - \frac{1}{2} h_j (t_j + t_{j-1}) = 0 \tag{26}$$

$$(1+2\gamma\eta)(q_j - q_{j-1}) + h_j \gamma (q_j + q_{j-1}) + \frac{A_1 A_2}{2} h_j (fq)_{j-\frac{1}{2}} - A_1 A_2 h_j p_{j-1}^2 - A_1 M p_{j-\frac{1}{2}} = 0$$

$$(27)$$

$$\left(A_3 + \frac{4}{3} Nr \right) [(1+2\gamma\eta)(t_j - t_{j-1}) + h_j \gamma (t_j + t_{j-1})] + (A_3 h_j \gamma t_{j-\frac{1}{2}}) + \frac{Pr}{2} \cdot A_4 h_j (ft)_{j-\frac{1}{2}} = 0$$

$$(28)$$

Equations (24) - (28), $j = 1, 2, \dots, J$, the boundary layer thickness η_J exceeds the edge of the boundary for extremely high values, the new boundary conditions are

$$f_0 = 0, p_0 = 1, \theta_0 = 1, p_J = 0, \theta_J = 0 \tag{29}$$

Newton's method.

Linearising the non-linear system (24)-(28), by using Newton's method, introduce

$$f_j^{(k+1)} = f_j^{(k)} + \delta f_j^{(k)}, p_j^{(k+1)} = p_j^{(k)} + \delta p_j^{(k)},$$

$$q_j^{(k+1)} = q_j^{(k)} + \delta q_j^{(k)},$$

temperature is an increasing function of parameter B_i , we have the stronger convection results for high surface temperatures which leads to go deeper into the stagnant fluid. From Fig. (8), we noticed that magnitude of skin friction coefficient is directly proportional to the values of both the magnetic field parameter as well as magnetic nano particle volume fraction. Also remarked that the coefficient of drag skin friction is more for cylinder than that of flat plate. Here the negative value of coefficient of skin friction means the stretching cylinder employ a dragging force over the surface of the fluid and the positive values employ the opposite.

Fig. (9) shows that drag Nusselt number (rate of heat transfer) is inversely proportional to the magnetic field parameter, however it is directly proportional to the magnetic nano particle volume fraction. It's true, since the thermal conductivity increases with nano particle volume fraction. This implies the acceleration of heat transfers rate entire the boundary layer. Increase in both thermal radiation parameter and the convective heating parameter shows increase in drag Nusselt number.

In table 3, we compared the results across magnetic and non magnetic nano particles. Here we have chosen Al_2O_3 as non magnetic nano particle. Thermal conductivity of Al_2O_3 is 40 W/m-k. Because Al_2O_3 is having high thermal conductivity, than magnetic nano particles, and Nusselt numbers of Al_2O_3 are high even in the absence of magnetic field. When magnetic field strength is increased all the magnetic nano particles arranged into same direction and comparatively show higher heat transfer rates, like non magnetic nano particle Al_2O_3 . This collation shown in table 3.

The heat transfer rate is high for Al_2O_3 when compared with that of magnetic nano particles when there is no magnetic field. Almost a percent difference between magnetic and non magnetic nano particles increase by increasing solid volume fraction of nano particles. When magnetic field strength is increased the magnetic nano particles join themselves, also the percent difference with Al_2O_3 decreases.

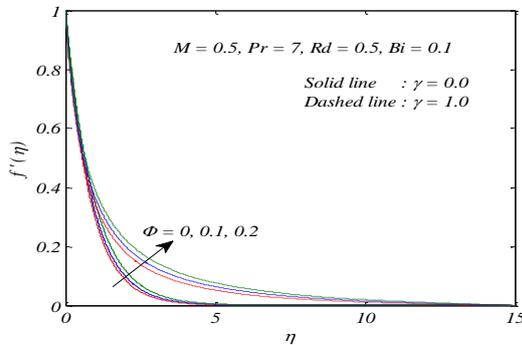


Fig. 2: Velocity profiles $f'(\eta)$ under different Φ

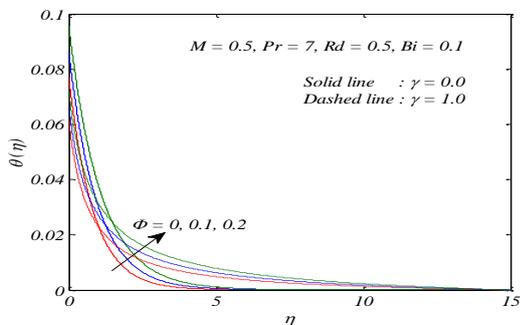


Fig. 3: Temperature profiles $\theta(\eta)$ under different Φ

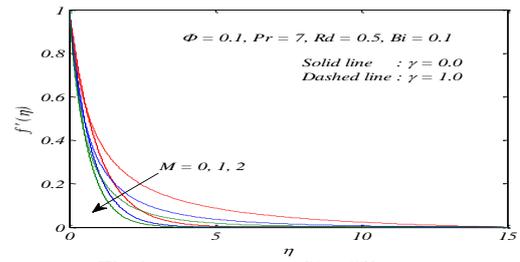


Fig.4: Temperature profiles different

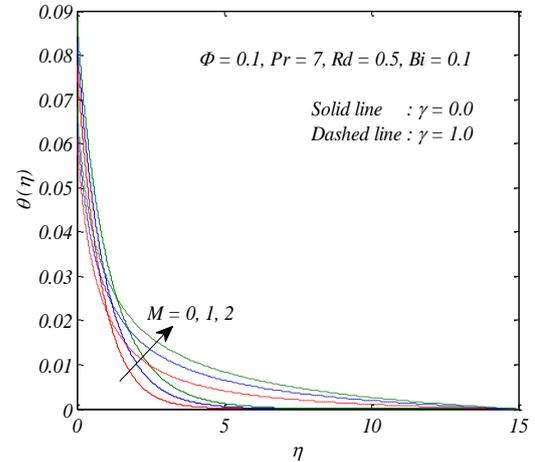


Fig. 5: Temperature profiles $\theta(\eta)$ under different M

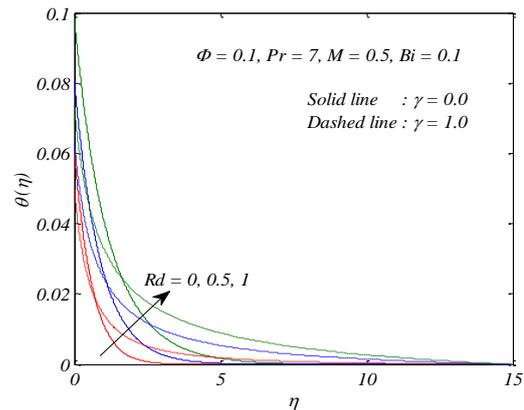


Fig. 6: Temperature profiles $\theta(\eta)$ under different Rd

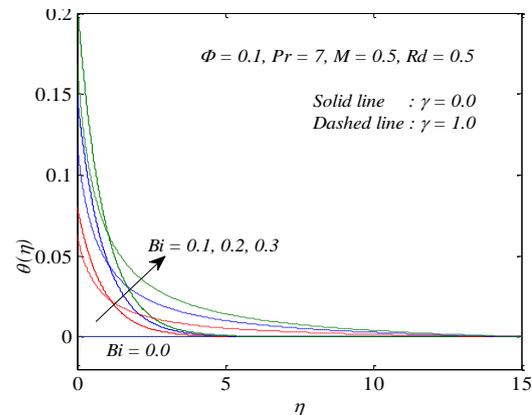


Fig. 7: Temperature profiles $\theta(\eta)$ under different Bi

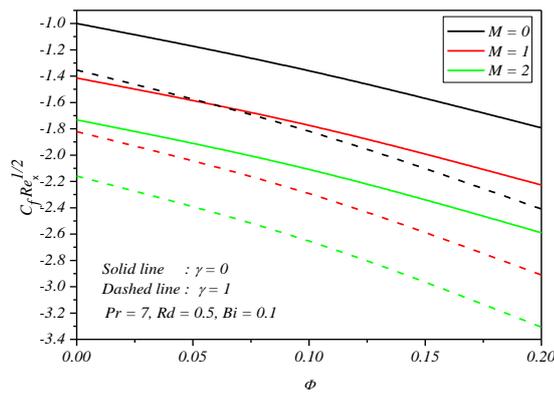


Fig. 8: $C_f Re_x^{1/2}$ under different values of M & Φ

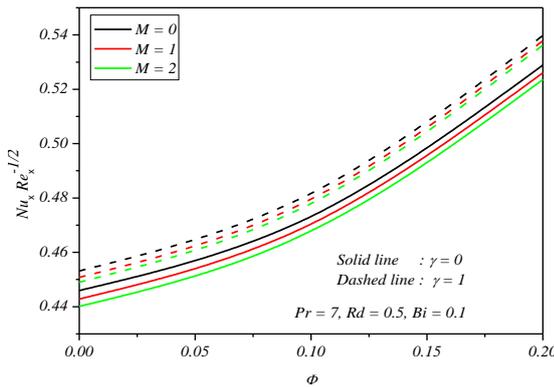


Fig. 9: $Nu_x Re_x^{-1/2}$ under different values of M & Φ

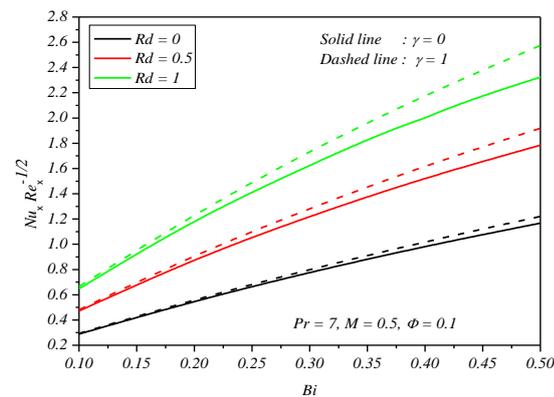


Fig. 10: $Nu_x Re_x^{-1/2}$ under different values of Rd & Bi

Table 1: Thermalphysical properties of base fluid/water and nanoparticle/magnetite [19, 20].

Physical properties	Water/base fluid	Magnetite/Magnetic	Al2O3/Non-magnetite
$\rho(kg / m^3)$	997	5180	3970
$c_p(J / kg K)$	4179	670	765
$k(W / m K)$	0.613	9.7	40

Table 2: Comparison of $f''(0)$ for different values of M in the absence of Φ for clear fluids.

M	Akbar et al. [36]	Salahuddin et al. [37]	Malik et al. [38]	Present output
0	1	1	1	1
0.5	-1.11803	-1.11801	-1.118105	-1.11803399
1	-1.41421	-1.41418	-1.14415	-1.41421356
5	-2.44949	-2.44942	-2.44947	-2.44948974
10	-3.31663	-3.31656	-3.31696	-3.31662479
100	-10.04988	-10.04981	-10.04983	-10.04987562
500	-22.38303	-22.038293	-22.38284	-22.38302929
1000	-31.63839	-31.63846	-31.63851	-31.63858404

Table 3: Deviation of Nusselt numbers with magnetic field parameter and solid volume friction of magnetic and non – magnetic nanoparticles with $Pr = 7, Bi = 0.1, \gamma = 1$.

M	Φ	Magnetite/Magnetic	Al ₂ O ₃ /Non-magnetic	%
Difference with Al ₂ O ₃				
0	0	0.45315832	0.46573460	0.027003362
	0.05	0.46471046	0.48224043	0.03138648
	0.1	0.48169334	0.50627906	0.04856159
1	0	0.53984119	0.59063948	0.08600558
	0.05	0.45078048	0.46324207	0.02690082
	0.1	0.46250107	0.47984974	0.03615438
2	0	0.47960258	0.50393838	0.04829122
	0.05	0.53784817	0.58821499	0.08562655
	0.1	0.44902220	0.46140788	0.02684323
	0.05	0.46082836	0.47805819	0.02684323
	0.1	0.47798724	0.50215632	0.04813059
	0.2	0.53625599	0.58632160	0.08538933

5. Conclusions

The present study investigates the magneto hydrodynamic flow and heat transfer analysis of ferrofluid along a stretching cylinder with thermal radiation and convective heating. The main findings of the study are:

By considering the thermal radiation and convective heating on energy equation we tested the magnetic hydro dynamic flow of ferrofluid along a flat plate and stretched cylinder. The profiles of temperature, velocity, surface shear stress and Nusselt number are good in the case of stretching cylinder. On increasing the magnetic field parameter, both the velocity, heat transfer rate at the surface decreases.

There is a decrease in percent difference in heat transfer rate of magnetic nano particles along with Al₂O₃ when magnetic field strength is increased.

The heat transfer increases due to thermal radiation and convective heating.

Current results have good agreement with the previous results up to nine decimals.

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